

Title: Optimization of Heat Treatment Furnace Operation

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Abstract: This project models and optimizes operation of a heat treatment furnace department of a foundry. Heat treatment furnace operation involves different operational temperatures, durations and atmospheres. It is inherently a batch process, but may be modeled as a linear program. The objective is to develop a tool to allow a weekly operational plan providing operators with a cost optimal strategy. Two methods were developed, one was formulated using pounds of furnace capacity and one using furnace time as variables. Both methods provided solutions, but the furnace hours best represented the nature of the problem. The program solutions provide a method to lower operational costs while providing insight to the characteristics of the process. The program may be rerun for any changes such as equipment failure or new parts to run, and a new department operation plan developed.

OPTIMIZATION OF HEAT TREATMENT FURNACE OPERATION

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EMP-P92

Optimization

of

Heat Treatment Furnace Operation

By

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Heat Treatment Furnace Operation

Executive Summary

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A tool was developed using linear programming techniques to improve operation in the Precision Castparts Heat Treatment Department.

The production schedule for a particular week was analyzed and the optimal strategy for running the department was found.

The program provides guidance to load furnaces in the most cost effective manner. Forecast of the weekly schedule for operations, labor (leave and overtime), and maintenance is enhanced. It also provides a tool for Engineering to study future equipment additions or modifications. Trade offs in operating cost can be predicted for changes in schedule and product mix. Impact of additional workload or downtime can be forecast.

Introduction

The heat treatment department at Precision Castparts Corporations Small Structures Plant (SSBO) processes thousands of stainless steel alloy parts each month. The parts made include artificial joints and turbine blades to mention a few. The properties of these materials are critical. To achieve these properties treatments are required at temperatures from 1100 to 2200 degrees Fahrenheit, for times from 1 to 20 hours, in either atmospheric air, argon, or vacuum.

The department has a number of furnaces available. Some are exclusively for vacuum processing and others are for either atmospheric air or argon processing. The cost of department operations varies with the type of processing required and which furnace is selected for each processing operation. The furnaces differ in capacity and efficiency. Meeting delivery schedule is the primary goal forcing parts to be moved through the department quickly. This often forces a furnace to be run with less than a full load. A methodology to assist operators in determining which furnace to run how much of each process has the potential to save the company money and improve department operations. This is the goal of this project.

Figure 1 shows the layout of the heat treat area. The department has seven different furnaces. Some of these furnaces are more costly to operate since they operate at higher temperatures and with argon or vacuum atmosphere. The furnaces have different capabilities, capacities, and efficiencies. The vacuum furnaces only had three processes scheduled and the problem became trivial. This report will therefore examine only the air/argon furnaces in detail. The vacuum furnace solution is included in Appendix III.

The Problem

The problem is to schedule the furnaces to reduce processing cost while meeting production schedule.

Furnaces C18 and C25 operate in air or argon and at temperatures from 1200 to 2100 degrees Fahrenheit. Furnaces C10 and C30 operate in vacuum over the same temperature range and can quench parts with argon.

In formulation of our problem the furnaces are identified as follows:

Furnace #1 C18 air or argon processing

Furnace #2 C25 air or argon processing

Furnace #3 C10 vacuum processing

Furnace #4 C30 vacuum processing

Appendix #1 shows the furnace capabilities, capacities, operational costs etc.

Methodology

Two different methodologies were employed for solving this problem. They were then compared. The problem formulations were all of a transportation type problem (1,2,3,4,5).

In the first method, the objective variables were pounds of material processed. The a_{ij} coefficients were in hours per pound and the C_{ij} coefficients were in dollars per pound.

In the second method the objective variables are in hours, the a_{ij} coefficients are in units of pounds per hour for the demand constraints, and the C_{ij} coefficients are in units of dollars per hour. This method is similar to that used by Chung (5, page 279) to create a transportation problem by using ratios of machine capacity.

Assumptions

Because of the batch nature of this process an initial difficulty was encountered.

The batch process lends itself to an integer solution. Reducing the number of batch runs will reduce cost. As an option we studied the calculation of a cost function of the pounds of material processed. This resulted in a non-linear problem. It was apparent that we would have to make certain assumptions to allow a linear program solution

Assumptions:

Method 1

The furnaces process material at a constant cost per pound regardless of percent capacity used. Therefore a half full batch costs the same per pound as a full batch to process. The time duration of each process was factored into the formulation.

Method 2

The assumption for this method is that batches are divisible at the same batch cost, but factors are included for partial batches in the derivation of the constraint coefficients.

Linear Program Conditions

It is important to verify that we have met the basic assumptions of linear programming:

1. Linearity and additivity. This assumption was key to simplify our program. For method 1, cost per pound is constant for each furnace and process. For method 2, cost per hour is constant. This is the key difference between the two methods.

- 2. Divisibility. The divisibility assumption applies because the problem was formulated in terms of pounds of material processed or hours of furnace operation, not batches. If this assumption could not be met the problem would have to be solved as an integer problem. If we had the tools to solve this type of problem in this manner we might be able to improve our solution.
- 3. Fitness or limited resources. There is finite number of furnaces and finite number of hours to process all the parts in the department, therefore this condition is met.
- 4. Deterministic. The variables do not change over the period of the study (one week).

Data Acquisition

Data for a typical production week was gathered. For furnaces 1 & 2, over 1200 parts were in the staging area waiting to be heat treated. There were 18 different heat treatment processes required for these parts. For furnaces 3 & 4, 135 parts required 3 different processes. Sample documentation showing process requirements and pounds per part are attached. See appendix II.

Parts mix varies from week to week. Studies could be run at the beginning of each week to give operators guidance to the most optimal method for the weeks operation.

Linear Program Formulation

Method 1

In order to avoid the integer/non-linear difficulties previously discussed, this problem was set up on a per pound basis.

The objective coefficients were computed for each of the 18 processes and for each furnace. Adjustments for different operating temperatures were then made to determine the furnace operating cost per hour (\$/hr) for each process. These are sumarized in appendix I. The objective coefficients were then calculated in units of dollars per pound as follows:

C_{ij} = Furnace operational cost per hour(\$/hr) x Cycle time(hrs) Furnace Capacity (lbs)

= dollars per pound (\$/lb)

These coefficients are only accurate for full furnace loads. Making the coefficients change with percent capacity results in a nonlinear problem. In this problem this assumption is justified as almost all furnace loads are near capacity due to the large number of parts in each process batch.

The constraints were then formulated for the time required to process parts in each of the furnaces. A limit of 5 days (3 shifts per days) was selected to process all the parts in order to meet delivery schedule. Each furnace has a capacity limit and the constraint was formulated with the coefficients in terms of pounds per hour. These were calculated for each furnace and each process as follows:

The variables (X_{ij}) are the pounds of each process to be processed in each furnace. The first subscript (1,2,3,4) is the furnace number. The second subscript (1 to 18 for argon/air, and 1 to 3 for vacuum) is the process number. For example; X_{214} is the pounds processed in furnace 2, of process 14.

The constraint equations are therefore:

- 1. The total hours available in furnace number 1
- 2. The total hours available in furnace number 2
- 3-21. The requirements to complete each required component.

All variables are non-negative.

It is a process scheduling problem. It is also similar to a transportation problem. We have a demand for parts and a supply of a resource (furnace time). In researching this problem we found similar problems in a number of sources. In a book by Chung(ref, page 279) there is a problem which has a number of machines which operate at different efficiencies are scheduled to process material in the most efficient manner. Machines are related in terms of their hourly production rates to make the problem a transportation problem. This is the same approach which we have taken.

Method 2

For this solution the problem was set up in a per hour basis.

The objective coefficients were computed for each furnace, at each process operation temperature. These are included in Appendix II.

 C_{ij} = operational cost in dollars per hour (@ operational temperature). = \$/lb

These coefficients are valid for either full loads or partial loads unlike method 1. The objective function totals operational costs from both furnaces.

The constraints are 1) total available furnace hours (supply), and 2) to for each process to total demand for each process.

The coefficients of the demand constraints were derived as follows:

 The total pounds of each process was divided by the furnace capacity, then rounded up to make whole "batches".

- 2. The "batches" was multiplied by the hours per batch.
- 3. The total pounds to be processed was divided by total hours (2).

The units of the "batches" (lb/lb) is dimensionless. Then multiplied by hours (units hours). Total pounds divided by this number then yields pound per hour.

d = Integer(lbs matl to be processed/furnace capacity)

 $a_{ij} = \underline{\text{total lbs to be processed in this process}}$ d * hours/ batch

The variables (X_{ij}) are the hours of furnace time for each process, for each furnace. The first subscript (1,2,3,4) is the furnace number. The second subscript (1 to 18 for argon/air, and 1 to 3 for vacuum) is the process number. For example; X_{214} is the hours in furnace 2, of process 14.

The constraint equations are therefore:

- 1. The total hours available in furnace number 1
- 2. The total hours available in furnace number 2
- 3-21. The requirements to complete each required component.

All variables are non-negative.

Note: these are the same as in method 1.

LINDO

The linear programs were solved using LINDO (6). The solution for the method 1 problem was obtained in 6 iterations for the air/argon problem and in 6 iterations for the vacuum processed parts (see Appendix III). The method 2 solution was run for the air/argon processes only and gave a solution in 7 steps.

A warning message was given by LINDO for the method 1 air/argon processed parts. The two first constraint equations were multiplied on both sides by 10 to better scale the problem.

The Solution By Method 1

LINDO gave a solution to the problem as follows:

Furnace #1

	Process	Pounda	S
	5	1943	
	6	459	
	7	462	
	8	3460	
	9	525	
	18	639	
Furnace #2			
	1,	14707	
	2	1318	
	3	10964	
	4	669	
	8	823	
	10	2333	
	11	2618	
	12	1314	
	Process		Pounds
	13		2770
	14		1046
	15		2142
	16		578
	17		2003

The objective function value is \$3015.35.

Looking at the results we see that only process 8 is split between the two furnaces. As expected furnace #2 is preferred as it has the lower cost per pound. The capacity of furnace #2 is entirely used up, and furnace #1 has over 37 hours available. This indicates what reserve capacity this department has.

Solution by Method 2

LINDO produced the following solution for the problem when the problem was constructed on an hours basis and the total weekly available furnace hours was held to 130 each:

ce #1	
Process	Hours
4	5
5	55.2
6	21
7	3.8
10	12.3
16	5.1
17	3.86
18	4.0
re #2	
Process	Hours
1	40
2	3.5
3	35.2
8	12
11	8.8
12	3.5
13	7.6
14	4.3
15	10
17	5
	Process 4 5 6 7 10 16 17 18 ee #2 Process 1 2 3 8 11 12 13 14 15

The value of the objective function is \$3595.08.

Sensitivity Analysis

METHOD 1

SHADOW PRICES. Furnace one has a surplus of 37.9 (379.4 in equation due to scaling) hours which can be used for processing. The shadow price for this constraint is therefore zero. Any additional processing should be done in Furnace one until the surplus is exhausted.

The shadow price for an additional hour of furnace two is \$9.40. This tells us that for each additional hour of use of furnace two should cost us less than \$9.40 to operate the furnace or adding the additional resources is not profitable.

The shadow prices of the remaining constraints (weight constraints for processes 1-18) are the cost per pound to process an aditional pound of material. For example, the shadow price for process 6 from the LINDO run is \$0.315/lb.

RANGE ON THE OBJECTIVE FUNCTION COEFFICIENTS. The objective function ranges show how the price per pound can decrease or increase by the indicated amount without changing the solution. For instance, the cost per pound of furnace one, process 5 can increase \$0.054 before requiring a new solution to the problem. It can also decrease to zero.

RANGE ON RIGHTHAND SIDE COEFFICIENTS. For constraints one and two (time constraints on furnaces one and two respectively), the right hand side ranges show how much additional time could be made available for a particular furnace before the optimal solution would change. For furnace one, the amount of available time could increase to infinity (due to the fact that there is slack) and the available time could decrease 37.94 hours and the given solution would still remain optimal.

For furnace two, the amount of available time could increase 9.206 hours and decrease 2.189 hours and the given solution would remain optimal.

The right hand side ranges for the remaining constraints (weight constraints on processes 1 through 18) tell us the range of weights for which the given solution remains optimal. For example for process 15, the amount of material could range from 0 to 2799.474 lbs and the solution remains unchanged. Note that all processes except 1, 3, and 8 can decrease to zero and the solution does not change.

SENSITIVITY ANALYSIS FOR METHOD 2

The sensitivity analysis is very similar to that for method one. The slack in furnace 1 is 10.78 hours and the shadow price for furnace 2 is \$5.00 per hour. The objective coefficient ranges give an indication of the impact of a cost increase (perhaps due to labor or energy) and its affects on the solution. The right hand side coefficients show how either available furnace hours or pounds of each process can be varied without changing the solution. This is discussed above in the method 1 analysis.

Discussion

These results are for a "snapshot" of a particular week of data and can deviate significantly in other weeks. The value of this program is the insight that it gives in understanding the availability of resources and the impacts of various process\parts mixes on that.

Without this information operators might load parts into any available furnace. The solution specifies which process goes in which furnace. Without this planning tool parts might be loaded in a less cost effective manner or in a manner which won't meet production schedule.

Sensitivity analysis showed slack in furnace one for both methods. This would assist the shift supervisor in scheduling labor, knowing how much labor/furnace surplus is available for the week.

Scheduling maintenance on equipment could also be done using the slack. This would maintain optimal schedule and not require overtime for maintainance. If maintenance requirements exceed slack time a new solution could be run and new schedule created.

Both methods produced a solution with similar objective function values. The assumptions did drive processes into different furnaces. As method 1 assumed a continuous process it deviated more from the batch nature of the solution. It did not yield correct furnace hour impacts however. If the batch nature of the processes is reintoduced into the solution we find that the actual number of hour required on furnace one is 108 (vs 82) and 142 hours (vs 120). This is a significant deviation.

Method two tends to retain the batch nature in the solution and actually schedules total furnace resource time within a much closer margin. When time resources are reduced, more of the processes are forced into both furnaces, but with 130 hours per week available for each furnace(note method two showed that 120 hours per furnace per week was infeasible), only one process was forced into both furnaces. It did not correctly divide time resources between the furnaces, but it did schedule more time than needed so the work can be completed.

In terms of cost per pound, furnace 2 is much more efficient than furnace 1, so method 1 drove all the material towards that furnace. Without resource constraint all material goes to that furnace. Method 2 recognized that the smaller furnace 1 was more economical for batches within its capacity.

The more accurate method is method 2, however the most accurate would be to develop an integer solution which would fully recognize the batch characteristics of this process. Method two however provide a good solution of the problem.

Conclusions

A linear program can be developed to solve a batch type problem. Selection of the formulation can greatly affect the solution. Solutions found gave a reasonable plan for department operations. The process can be understood using this tool and decisions on department operational procedures, resource requirements, etc. can be better made.

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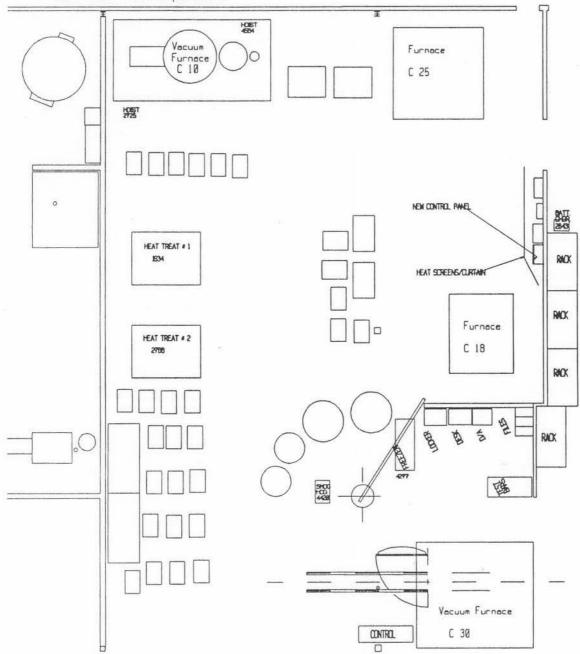


Figure 1 Heat Treatment Department Layout

	Solutions fo	or the Air/Arç	gon Furnace	s
Process	M1 F1	M1 F2	M2 F1	M2 F2
	lbs	lbs	hrs	hrs
1	0	14707	0	40
2	0	1318	0	3.5
3	0	10964	0	35.2
4	0	669	4.79	(
5	1943	0	55.2	(
6	459	0	20.96	(
7	462	0	3.8	(
8	3460	823	0	12
9	525	0	4	(
10	0	2333	12.2	(
11	0	2618	0	8.8
12	0	1314	0	3.5
13	0	2770	0	7.6
14	0	1046	0	4.3
15	0	2142	0	10
16	0	578	5.1	(
17	0	2003	3.86	5.03
18	639	0	4	(
	7488	43285	113.91	129.93

Figure 2 Comparision of Method 1 and Method 2 Results

Appendix I

Heat Treatment Furnace

Operational and Cost Data

EMGT 540 - Heat Treat Project Data - Furnace Cost Summary - 1700 (f)

Furnace	Furnace Name	\$/hr Labor	\$/hr Supplies	\$/hr Argon	\$/hr Repairs	\$/hr Electric	\$/hr Gas	\$/hr Total 14	Pounds Capacity 800
2	C18 C25	2	2	5	1	0	6 7	17	1500
3	C10	1	1	0	4	3	0	9	900
4	C30	2	1	1	4	4	0	12	1000

EMGT 540 - Heat Treat Project Data

		TEMP	CYCLE TIM	E		# OF			Furn 1	Furn 2	Furn 1	Fum 2	Fum 1	Fum 2
Process #	REF #	(deg F)	(HRS)	ATMOSPHE	PART #	PIECES	POUNDS/PIECE	POUNDS	\$/hr	\$/hr	\$/pound	\$/pound	hr/pound	hr/pound
****	*****	*****		****		*****	****	*****		*****	****			
1	1050	1750	4	argon	3154	1	93	93	14	17	0.07	0.045	0.005	0.00266
					3396	29	25	725						
					4493	12	30	360						
					5420	119	70	8,330						
					5882	18	150	2,700						
					6331	1	94	94						
					6511	1	140	140						
					7241	3	165	495						
					7266	1	38	38						
					7674	18	55	990						
					7856	2	195	390						
					8071	4	88	352						
							TOTAL POUNDS	14,707						
2	1051	1900	3.5	argon	3025	2	33	66	15	18	0.066	0.042	0.00438	0.00233
-					7438	2	44	88	100		0.000			
					7439	22	17	374						
					10309	6	45	270						
					10339	4	130	520						
							TOTAL POUNDS	1,318						
3	1052	2000	4.4	argon	3154	1	93	93	16	19	0.088	0.056	0.0055	0.00293
0.775	Liveren	2620		7.555	3396	28	25	700						
					3797	2	63	126						
					5420	117	70	8,190						
					5640	8	50	400						
					5882	4	150	600						
					7241	3	165	495						
					7680	3	120	360						
							TOTAL POUNDS	10,964						

EMGT 540 - Heat Treat Project Data

		TEMP	CYCLE TIMI	-		# OF				F 0		c o	F	
Process #	REF#	(deg F)	(HRS)	ATMOSPHE	PART #	PIECES	POUNDS/PIECE	POUNDS	Furn 1 \$/hr	Furn 2 \$/hr	Furn 1 \$/pound	Furn 2 \$/pound	Furn 1 hr/pound	Furn 2 hr/pound
*****	1361 #	(neg r)	(1110)	****							aypound	a/pound	m/pound	ni/pound
										57777	25000		(37737)	10000000
4	1053	2100	5	argon	4730	2	120	240	17	20	0.106	0.068	0.00625	0.00333
					5126	2	120	240						
					5730	3	13	39						
					10036	10	15	150						
							TOTAL POUNDS	669						
5	1162	1400	18.4	air	10435	29	67	1,943	8	10	0.184	0.123	0.023	0.01226
							TOTAL POUNDS	1,943						
6	1205	1325	21	argon	5655	17	27	459	12	15	0.315	0.21	0.02625	0.014
							TOTAL POUNDS	459						
							TOTAL FOUNDS	458						
7	1208	1400	3.8	argon	4973	2	71	142	12	15	0.057	0.038	0.00475	0.00253
					5662	4	80	320						
							TOTAL POUNDS	482						
8	1225	1750	4	argon	3293	252	17	4,284	14	17	0.07	0.045	0.005	0.00266
							TOTAL POUNDS	4,284						
9	1227	1750	4	argon	7084	5	105	525	14	17	0.07	0.045	0.005	0.00268
							TOTAL POUNDS	525						
10	1250	1900	4,1	argon	746	109	11	1,199	15	18	0.077	0.049	0.00512	0.00273
1.127.6	100000	0.0000	25.50		4730	1	120	120	40	25	2707530	2000	101011011071	
					5802	4	120	480						
					5128	2	120	240						
					5730	3	13	39						
					4730	1	120	120						
					10265	1	135	135						
							TOTAL POUNDS	2,333						

EMGT 540 - Heat Treat Project Data

Process #	REF#	TEMP (deg F)	CYCLE TIM (HRS)	E ATMOSPHE	PART #	# OF PIECES	POUNDS/PIECE	POUNDS	Furn 1 \$/hr	Furn 2 \$/hr	Furn 1 \$/pound	Furn 2 \$/pound	Furn 1 hr/pound	Furn 2 hr/pound
*****	*****	*****	*****	*****			*****	*****		*****		*****	*****	
11	1251	1900	4.4	argon	8126	22	119	2,618	15	18	0.083	0.053	0.0055	0.00293
							TOTAL POUNDS	2,618						
12	1264	1900	3.5	argon	746	109	11	1,199	15	18	0.066	0.042	0.00437	0.00233
					10506	1	115	115						
							TOTAL POUNDS	1,314						
13	1268	1925	3.8	argon	7680	4	120	480	15	18	0.071	0.048	0.00475	0.00253
				STORTS.	7481	19	110	2,090						
					7855	1	200	200						
							TOTAL POUNDS	2,770						
14	1280	2000	4.3	argon	90201	1	18	18	16	19	0.086	0.055	0.00537	0.00286
					7240	2	140	280						
					7084	6	105	630						
					7088	1	118	118						
							TOTAL POUNDS	1,046						
15	1282	2000	5	argon	3293	128	17	2,142	16	19	0.1	0.063	0.00625	0.00333
							TOTAL POUNDS	2,142						
16	1294	2100	5.1	argon	7457	1	131	131	17	20	0.108	0.068	0.00637	0.0034
1.5	1			wi Mari	10339	2	130	260	2.300	7.7	71177			
					7439	11	17	187						
							TOTAL POUNDS	578						

								-OUNDS/PIECE	POUNDS	Furn 1 \$/hr	S/hr	Fum 1 \$/pound	\$/pound	Furn 1 hr/pound	hr/pound
											_	<u></u>			-
	180														
		1432	1075	2.0		10405				70/26	000000	Tonasan.	7/2/2003	Van Statistisch	
		1402	1975	3.8	argon	10435 10436	24 5	67 79	1,608 395	16	19	0.076	0.048	0.00475	0.00253
								TOTAL POUNDS	2,003						
18		1433	1750	4	air	10407	11	42	462	10	12	0.05	0.032	0.005	0.00266
						10353	1	177	462 177						
								TOTAL POUNDS	639						

EMGT 540 - Heat Treat Project Data

		TEMP	CYCLE TIME			# OF			Furn 3	Furn 4	Furn 3	Furn 4	Fum 3	Furn 4
Process #	REF#	(deg F)	(HRS)	ATMOSPHE	PART #	PIECES	POUNDS/PIECE	POUNDS	\$/hr	\$/hr	\$/pound	\$/pound	hr/pound	hr/pound
	*****		*****	*****		****	*****							
1	1422	1750	9	vacuum	3688	9	47	423	9	12	0.09	0.108	0.01	0.000
					7443	8	45	360						
					4535	20	42	840						
							TOTAL POUNDS	1,623						
2	1436	1400	10.6	vacuum	10506	2	115	230	7	10	0.082	0.106	0.0117	0.0106
	1400	1400	10.0	Vacuum	7461	21	110	2,310		10	0.002	0.100	0.0117	0.0100
					90201	1	18	18						
					50201									
							TOTAL POUNDS	2,558						
3	1437	1925	9.8	vacuum	6964	8	290	1,740	10	13	0.109	0.127	0.011	0.0098
					7461	41	110	4,510						
					10084	9	205	1,845						
					10306	14	200	2,800						
					8071	4	88	352						
							TOTAL POUNDS	11,247						

LABOR EREAKDOWN

Furnace #1 & #2

Time To Load/Unload & Do Paperwork = 1 Hour

Avg Time/Furnace Cycle = 4.47

Labor Hrs/Furn Hr = 0.22

Furnace #8

= 0.5 Unload/Load Time/Furn Cycle = 4.3 Furn Labor Hrs/Furn Hr Ratio Labor Hrs/Furn Hr = 0.12 #1 0.220 0.69 #2 0.220 0.69 #8 0.116 0.36 #10 0.185 0.58 Furnace #10 0.266 0.83 #25 0.319 1.00 Unload/Load 0.313 1.00 New Avg Time/Furn Cycle = 8.1

Furnace #18

Unload/Load = 1.25
Avg Time/Furn Cycle = 4.7
Labor Hrs/Furn Hr = 0.266

Labor Hrs/Furn Hr = 0.185

Furnace #25

Unload/Load = 1.5 Time/Furn Cycle = 4.7 Labor Hrs/Furn Hr = 0.319

New Furnace #4 30

Unload/Load = 1.5 Time/Furn Cycle = 4.8 Labor Hrs/Furn Hr = 0.313

FURNACE COST DATA

EXPECTED MAINTENANCE COSTS

FURN #	COST	RATIO
#1	\$ 4,000	0.33
# 2	4,000	0.33
# 8	1,000	0.08
#10	50,000	4.17
#18	12,000	1.00
#25	12,000	1.00
NEW	24,000	2.00

FURNACE COST DATA }

ELECTRICAL CONSUMPTION CALC.

Furnace #1 & #2 Heater Capacity = 120KW Motors = 4 HP or 3KW/Hour

										Time/Cycle	KW
To	Temp	Furnace	at	70%	or	84	+	3	KW/H	1.53	133.1
At	Temp	Furnace	at	25%	or	30	+	3	KW/H	2.94	97.0
										-	
Av	KW/I	Hour = 5	1.5							4.47	230.1

Furnace #18 Blowers = 4HP or 3KW/Hour # #25 # = 5HP or 3.7KW/Hour

Furnace #10

To Temp 25v x 3400 amps x 1.73 = 147.1KW/Hour At Temp (Avg) 15v x 1700 amps x 1.73 = 44.1KW/Hour Pumps Operate Through Cycle (21HP) or 15.7KW/Hour

		Time/Cycle	KW
Pump Down	15.7 KW/Hour	1.8	28.3
Heat Up	147.1 + 15.7	1.8*	293.0
At Temp	44.1 + 15.7	2.8**	167.0
Cool Down	15.7	2.2	34.5
Avg = 60.8 I	(W/Hour	8.6	523.0

^{*} Furn reaches temp in avg. of 1.8 hours load takes longer ** Includes some load heat up time

Electrical Consumption.

Furnace	#1	51.5	KW/Hour		13.91
	#2	51.5	KW/Eour		13.91
	#10	60.8	KW/Eour		16.40
	\$ 18	3.0	KW/Eour		0.81
	#25	3.7	KW/Eour		1.00
EST.	NEW	75.0	KW/Eour	*	20.20

ESTIMATED SUPPLY COST/YR

FURN #	FIXTURES BASKETS	TC	ARGON*	TOTAL	RATIO TO \$25
#1	2,500	11,000		13,500	0.23
#2	2,500	11,000		13,500	0.23
#8		1,000		1,000	0.017
#10	7,000	11,000		18,000	0.31
#18	31,200	11,000		42,200	0.73
#25	46,800	11,000		57,800	1.00
NEW # C30	7,000	11,000		18,000	0.31

^{*}See Derivation Below Will Be Separate

ARGON USE/CYCLE

- #10 Backfill to -5 in Hg then maintain level while cooling. Before unloading, equalize to atmosphere pressure with Argon. This procedure uses argon equivalent to the chamber volume; or 57.75 ft. On an operating basis this is 7.1 ft /furn hour (57.75/8.1)
- \$18 Purge for one hour at 150 scfh, run in furnace for an average of 4.7 hours at 120 scfh, and cool for an avg. of 0.5 hours at 120 scfh. Total Argon used/cycle is 774 scf. On a furnace hour basis this is 774/4.7 or 165 ft furn hour.
- #25 Purge for two hours at 150 scfh, run for 4.7 hours at 120 scfh, and cool for an avg. of 0.5 hours at 120 scfh. Total Argon used/cycle is 924 scf. or 197 ft / furn hour.

NEW Estimated use is 100 ft 3/cycle or 21.3 ft 3/furn hour.

FURN #	FT ³ /FURN HOUR	RATIO TO #25
#10	7.1	0.04 .
#18	165.0	0.84
#25	197.0	1.00
NEW	21.3	0.11

GAS CONSUMPTION

Only furnaces \$18 & \$25 use gas. BTU rating of \$18 is 1,800,000 BTU/HR & \$25 is 2,000,000/HR 1,800,000/2,000,000 = 0.90

FURNACE	RATIO TO #2	5
#18	0.90	
#25	1.00	

RENT

Rent is for fork trucks. Fork trucks are not used for the vacuum furnaces or freezer. Fork truck rent should be divided equally between remaining furnaces (furnace hours will determine apportionment).

SALARY & FRINGE

Divided equally between all furnaces (furnace hours will determine apportionment).

cc: Art Greenwood George Harriman Bob McClelland Bob McGinley Terry Spaulding

MM/tlg Clack/x505

FURNACE COST DATA }

Appendix II
Sample Week
Heat Treatment Department
Production Schedule

JOB DBERNT29 SFSOB1.

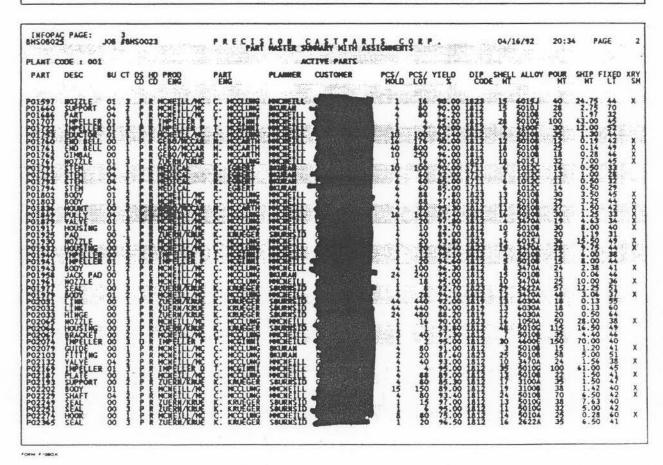
PRECISION CA PARTS CORP. MSGNUM DISPAICH LIST HI TMP HEAT TREAT

04/22/92

11:07

	PLANT: SE		7				江 草点							
	DUE OUT OPER	PART	JOB		EXPEDITE PRIORITY	JOB STATUS	PART	PART	NBR PCS	DAYS IN W/C	JOB DUE DATE	JOB STD HRS	SETUP HRS	CURR/WC
	05/14/92													
	14017	10436	0006-02	1162	20-SMP	21-SCHED	STRUT ÉND	CURT RUND	4	1	05/15/92	1.3		нтнтр
							TOTALS	FOR DATE	4			1.3	0.0	
•	05/21/92													
	14017	10435	0388-03	1162		21-SCHED	STRUT END	CURT RUND	8	1	05/26/92	2.7		HTHTP
							TOTALS	FOR DATE	8			2.7	0.0	
	03/19/92													
	14013	05655	0087-07	1205		25-R	BRACKET	C. MCCLUNG	4	1	04/10/92	0.1		HTHTP
							TOTALS	FOR DATE	4			0.1	0.0	
	04/22/92													
	14013	05655	0087-02	1205		24-F	BRACKET	C. MCCLUNG	13	1	05/14/92	0.4		нтнтр
							TOTALS	FOR DATE	13			0.4	0.0	
	04/15/92													
	14013	04973	0004-02	1208	20-SMP	24-F	IMPELLER	T. MCGINNI	2	2	04/24/92	5.3		HTHTP
							TOTALS	FOR DATE	2			5.3	0.0	
	05/12/92													
	14011	05662	0231-01	1222		21-SCHED	нив	M. MCCARTH	2	12	05/15/92	1.0		HTHTP
			0231-03	1222		21-SCHED	HUB	M. MCCARTH	1	1	05/15/92	0.5		HTHTP
		05002	0232-03	1222		21-SCHED	HUB	M. MCCARTH		1	05/18/92	0.5		нтнтр
							TOTALS	FOR DATE	4			2.0	0.0	
	04/16/92													
	14011	03293	0035-01	1225		21-SCHED	LUG	K. KRUEGER	126	1	05/07/92	0.0		нтнтр
							TOTALS	FOR DATE	126			0.0	0.0	

INFOPAC PAGE: JOS 2 1005.0023 PRECISION CASTPARTS CORP. 04/16/92 ACTIVE PARTS DESC BU CT OS HE PERE CUSTOMER LOT LOT ALERO DIP SHELL الشفينية والمنافئة والمنا 8533448834883555866643484348443486534665534883333485 Consequence of the second seco poodédi THE PERSON OF LAND SELECTION O ğ X X



SPART WEIGHT DATAS EXAMPLE 1 OF 1

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Page	OF	HEAT TREAT	REFERENCE	LIST BY	REFERENC	E NUMBER		27 FEB 92	07:49						
REF#		HRSATTEMP	ATMOS MEDI		TOTEMPI	ATTEMP1	QCH- MED2	COOLRT2	TOTEMP2	ATTEMP2	QCH- MED3	COOLRT3	TOTEMP3	ATTEMP3	DEWPT
1000	- 1		AIR AIR	0	0	0.00		0	0	0.00		0	0	0.00	0
1001	900	1.50	AIR AIR	0	70	0.00		0	0	0.00		0	0	0.00	0
1002	925	1.50	AIR AIR	0	70	0.00		0	0	0.00		0	0	0.00	0
1003	1000	1.50	COMMENTS AIR AIR COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0
1004	1050	1.50	AIR AIR COMMENTS	0	70	0.00	÷.	0	0	0.00		0	0	0.00	0
1005	1100	1.50	AIR AIR COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0
1006	1125	1.50	AIR AIR COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0
1007	1150	1.50	AIR AIR COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0
1008	1150	4.00	AIR AIR	0	70	0.00		0	0	0.00		0	0	0.00	0
1009	1150	16.00	AIR AIR COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0
1010	1200	2.00	AIR AIR COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0
1011	1325	8.00	AIR FUR	0	1150	8.00	AIR	0	120	0.00		0	0	0.00	0
1050	1750	1.00	ARG FCR	0	120	0.00		0	0	0.00		0	0	0.00	0
1051	1900	0.50	ARG FCR	0	70	0.00		0	0	0.00		0	0	0.00	0
1052	2000		ARG FCR COMMENTS	0	120	0.00		0	0	0.00		0	0	0.00	0
1053	2100		ARG FCR COMMENTS		70	0.00		0	0	0.00		0	0	0,00	0
1080	1350		COMMENTS		120	0.00		0 '	0	0.00		0	0	0.00	0
1100	450		COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1101	500		AIR AIR COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1102	625		AIR AIR COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1103	900		COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1104	900		COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1105	900		COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
	925		COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1107	925		COMMENTS		70	0.00		0	0	0.00		0	0	0.00	0
1108	925	4.00	COMMENTS	0	70	0.00		0	0	0.00		0	0	0.00	0

Appendix III Vacuum Furnace Solution

MIN 0.01 X31 + 0.008 X32 + 0.012 X33 + 0.012 X41 + 0.01 X42 + 0.014 X43

SUBJECT TO

- 2) 0.01 X31 + 0.0117 X32 + 0.011 X33 <= 120
- 3) 0.009 X41 + 0.0106 X42 + 0.0098 X43 <= 120
- 4) X31 + X41 = 1623
- 5) X32 + X42 = 2558
- 6) X33 + X43 = 11247

END

LP OPTIMUM FOUND AT STEP 6

OBJECTIVE FUNCTION VALUE

1) 180.40070

VARIABLE	VALUE	REDUCED COST
X31	1623.000000	.000000
X32	.000000	.000127
X33	9433.637000	.000000
X41	.000000	.000182
X42	2558.000000	.000000
X43	1813.364000	.000000

ROW SLACK OR SURPLUS DUAL PRICES

- 2)
 .000000
 .181818

 3)
 75.114230
 .000000

 4)
 .000000
 -.011818

 5)
 .000000
 -.010000

 6)
 .000000
 -.014000
- NO. ITERATIONS= 6

RANGES IN WHICH THE BASIS IS UNCHANGED:

11247.000000

	OBJ COEF	FICIENT RANGES	3
VARIABLE	CURRENT	T ALLOWAB	LE ALLOWABLE
	COEF INC	REASE DEC	REASE
X31	.010000	.000182	INFINITY
X32	.008000	INFINITY	.000127
X33	.012000	.000120	.000200
X41	.012000	INFINITY	.000182
X42	.010000	.000127	INFINITY
X43	.014000	.000200	.000120
	RIGHTHA	ND SIDE RANGE	S
ROW	CURRENT	ALLOWABLE	ALLOWABLE
	RHS INC	REASE DECI	REASE
2	120.000000	19.947000	84.311890
3	120.000000	INFINITY	75.114230
4	1623.000000	8431.190000	1623.000000
5	2558.000000	7086.249000	2558.000000

7664.718000 1813.364000

Appendix IV LINDO Solution Method 1

```
MIN 0.07 \times 11 + 0.066 \times 12 + 0.088 \times 13 + 0.106 \times 14 + 0.184 \times 15
   + 0.315 X16 + 0.057 X17 + 0.07 X18 + 0.07 X19 + 0.077 X110
   + 0.08299999 X111 + 0.066 X112 + 0.071 X113 + 0.086 X114 + 0.1 X115
   + 0.108 X116 + 0.07599999 X117 + 0.05 X118 + 0.045 X21 + 0.042 X22
   + 0.056 X23 + 0.066 X24 + 0.123 X25 + 0.21 X26 + 0.038 X27 + 0.045 X28
   + 0.045 X29 + 0.049 X210 + 0.053 X211 + 0.042 X212 + 0.046 X213
   + 0.055 X214 + 0.063 X215 + 0.068 X216 + 0.048 X217 + 0.032 X218
SUBJECT TO
    2) 0.05 X11 + 0.0438 X12 + 0.055 X13 + 0.0625 X14 + 0.23 X15
   + 0.2625 X16 + 0.0475 X17 + 0.05 X18 + 0.05 X19 + 0.0512 X110
   + 0.055 X111 + 0.0437 X112 + 0.0475 X113 + 0.0537 X114 + 0.0625 X115
   + 0.06369999 X116 + 0.0475 X117 + 0.05 X118 <= 1200
    3) 0.0266 X21 + 0.0233 X22 + 0.0293 X23 + 0.0333 X24 + 0.1226 X25
   + 0.14 X26 + 0.0253 X27 + 0.0266 X28 + 0.0266 X29 + 0.0273 X210
   + 0.0293 X211 + 0.0233 X212 + 0.0253 X213 + 0.0286 X214 + 0.0333 X215
   + 0.034 X216 + 0.0253 X217 + 0.0266 X218 <= 1200
   4) X11 + X21 = 14707
   5) X12 + X22 = 1318
   6) X13 + X23 = 10964
   7) X14 + X24 = 669
   8) X15 + X25 = 1943
   9) X16 + X26 = 459
   10) X17 + X27 = 462
   11) X18 + X28 = 4284
   12) X19 + X29 = 525
   13) X110 + X210 = 2333
   14) X111 + X211 = 2618
   15) X112 + X212 = 1314
   16) X113 + X213 = 2770
   17) X114 + X214 = 1046
   18) X115 + X215 = 2142
   19) X116 + X216 = 578
   20) X117 + X217 = 2003
   21) X118 + X218 = 639
END
```

LP OPTIMUM FOUND AT STEP

OBJECTIVE FUNCTION VALUE

1) 3015.3460

VARIABL	E VALUE	REDUCED COST
X11	.000000	.000000
X12	.000000	.002102
X13	.000000	.004462
X14	.000000	.008703
X15	1943.000000	.000000
X16	459.000000	.000000
X17	462.000000	.000000
X18	3460.921000	.000000
X19	525.000000	.000000
X110	.000000	.002342
X111	.000000	.002462
X112	.000000	.002102
X113	.000000	.001222
X114	.000000	.004120
X115	.000000	.005703
X116	.000000	.008045
X117	.000000	.004222
X118	639.000000	.000000
X21	14707.000000	.000000
X22	1318.000000	.000000
X23	10964.000000	.000000
X24	669.000000	.000000
X25	.000000	.054226
X26	.000000	.026579
X27	.000000	.004778
X28	823.078900	.000000
X29	.000000	.000000
X210	2333.000000	.000000
X211	2618.000000	.000000
X212	1314.000000	.000000
X213	2770.000000	.000000
X214	1046.000000	.000000
X215	2142.000000	.000000
X216	578.000000	.000000
X217	2003.000000	.000000
X218	.000000	.007000

ROW	SLACK OR S	SURPLUS	DUAL PRICES
2)	379.431400	.000000)
3)	.000000	.939850	
4)	.000000	070000	
5)	.000000	063898	
6)	.000000	083538	
7) 8)	.000000	097297	
8)	.000000	184000	
9)	.000000	315000	
10)	.000000	057000	
11)	.000000	070000	
12)	.000000	070000	
13)	.000000	074658	
14)	.000000	080538	
15)	.000000	063898	
16)	.000000	069778	
17)	.000000	081880	
18)	.000000	094297	
19)	.000000	099955	
20)	.000000	071778	
21)	.000000	- 050000	

NO. ITERATIONS= 6

RANGES IN WHICH THE BASIS IS UNCHANGED:

The said law	The second second			
OBI	COEFFI	CIENT	RANGES	
11111	1 1 1 1 1 1 1 1	L . I I I I I I	DOMESTICAL AND ADDRESS OF THE PARTY OF THE P	

VARIABI	LE CUR	RENT ALLO	OWABLE ALLOWABLE	ì
	COEF	INCREASE	DECREASE	
X11	.070000		.000000	
X12	.066000	INFINITY	.002102	
X13	.088000	INFINITY	.004462	
X14	.106000	INFINITY	.008703	
X15	.184000	.054226	INFINITY	
X16	.315000	.026579	INFINITY	
X17	.057000	.004778	INFINITY	
X18	.070000	.0000000	.000000	
X19	.070000	.000000	INFINITY .002342 .002462	
X110	.077000	INFINITY	.002342	
X111	.083000	INFINITY	.002462	
X112	.066000	INFINITY	.002102	
X113	.071000	INFINITY	.001222	
X114	.086000	INFINITY	.004120	
X115	.100000	INFINITY	.005703	
X116	.108000	INFINITY	.008045	
X117	.076000			
X118	.050000		INFINITY	
X21	.045000		INFINITY	
X22	.042000		INFINITY	
X23	.056000	4 TO 10 TO 1	INFINITY	
X24	.066000		INFINITY	
X25	.123000		.054226	
X26	.210000			
X27	.038000			
X28	.045000		.000000	
X29	.045000		.000000	
X210	.049000		INFINITY	
X211	.053000		INFINITY	
X212	.042000		INFINITY	
X213	.046000		INFINITY	
X214	.055000	.004120	INFINITY	
X215		.005703	INFINITY	
X216		.008045	INFINITY	
X217	.048000		INFINITY	
X218	.032000	INFINITY	.007000	

RIGHTHAND SIDE RANGES

		HAND SIDE KA	
ROW			ABLE ALLOWABLE
			DECREASE
2	1200.000000	INFINITY	379.431400
3	1200.000000	92.060500	21.893900
4	14707.000000	823.078900	3460.921000
5	1318.000000	939.652300	1318.000000
6	10964.000000	747.231900	3141.996000
7	669.000000	657.474400	669.000000
8	1943.000000	1649.702000	1943.000000
9	459.000000	1445.453000	459.000000
10	462.000000	7988.030000	462.000000
11	4284.000000	7588.628000	3460.921000
12	525.000000	7588.628000	525.000000
13	2333.000000	801.974200	2333.000000
14	2618.000000	747.231900	2618.000000
15	1314.000000	939.652300	1314.000000
16	2770.000000	865.371500	2770.000000
17	1046.000000	765.520900	1046.000000
18	2142.000000	657.474400	2142.000000
19	578.000000	643.938100	578.000000
20	2003.000000	865.371500	2003.000000
21	639.000000	7588.628000	639.000000

Appendix V LINDO Solution Method 2

```
MIN 14 X11 + 17 X21 + 15 X12 + 18 X22 + 16 X13 + 19 X23 + 17 X14
  + 20 X24 + 8 X15 + 10 X25 + 12 X16 + 15 X26 + 12 X17 + 15 X27 + 14 X18
  + 17 X28 + 14 X19 + 17 X29 + 15 X110 + 18 X210 + 15 X111 + 18 X211
  + 15 X112 + 18 X212 + 15 X113 + 18 X213 + 16 X114 + 19 X214 + 16 X115
  + 19 X215 + 17 X116 + 20 X216 + 16 X117 + 19 X217 + 10 X118 + 12 X218
SUBJECT TO
   2) X11 + X12 + X13 + 2 X14 + X15 + X16 + X17 + X18 + X19 + X110
  + X111 + X112 + X113 + X114 + X115 + X116 + X117 + X118 <= 130
   3) X21 + X22 + X23 + X24 + X25 + X26 + X27 + X28 + X29 + X210
  + X211 + X212 + X213 + X214 + X215 + X216 + X217 + X218 <= 130
   4) 193 X11 + 367 X21 = 14707
   5) 188.3 X12 + 376.6 X22 = 1318
   6) 178 X13 + 311.5 X23 = 10964
   7) 133.8 \times 14 + 133.8 \times 24 = 669
   8) 35.2 X15 + 52.8 X25 = 1943
   9) 21.9 X16 + 21.9 X26 = 459
   10) 121.57 X17 + 121.57 X27 = 462
   11) 178.5 X18 + 357 X28 = 4284
   12) 131.25 X19 + 131.25 X29 = 525
   13) 189.67 X110 + 284.51 X210 = 2333
   14) 148.75 X111 + 297.5 X211 = 2618
   15) 187.7 X112 + 375.4 X212 = 1314
   16) 182.2 X113 + 364.5 X213 = 2770
   17) 121.6 X114 + 243.3 X214 = 1046
   18) 142.6 X115 + 214.2 X215 = 2142
   19) 113.3 X116 + 113.3 X216 = 578
   20) 175.7 X117 + 263.5 X217 = 2003
```

LP OPTIMUM FOUND AT STEP

END

21) 159.75 X118 + 159.75 X218 = 639

OBJECTIVE FUNCTION VALUE

1) 3595.0820

VARIABLE	VALUE	REDUCED COST
X11	.000000	2.432912
X21	40.073570	.000000
X12	.000000	3.502276
X22	3.499734	.000000
X13	.000000	2.288316
X23	35.197430	.000000
X14	5.000000	.000000
X24	.000000	7.995447
X15	55.198860	.000000
X25	.000000	2.995448
X16	20.958900	.000000
X26	.000000	7.995447
X17	3.800280	.000000
X27	.000000	7.995447
X18	.000000	3.002276
X28	12.000000	.000000
X19	4.000000	.000000
X29	.000000	7.995447
X110	12.300310	.000000
X210	.000000	.495052
X111	.000000	3.502276
X211	8.800000	.000000
X112	.000000	3.502276
X212	3.500267	.000000
X113	.000000	3.505430
X213	7.599451	.000000
X114	.000000	4.007208
X214	4.299219	.000000
X115	.000000	.025439
X215	10.000000	.000000
X116	5.101501	.000000
X216	.000000	7.995447
X117	3.856054	.000000
X217	5.030327	.000000
X118	4.000000	.000000
X218	.000000	6.995447

ROW	SLACK OR	SURPLUS	DUAL PRICES
2)	10.784090	.000000	
3)	.000000	4.995447	
4)	.000000	059933	
5)	.000000	061061	
6)	.000000	077032	
6) 7) 8)	.000000	127055	
8)	.000000	227273	
9)	.000000	547945	
10)	.000000	098709	
11)	.000000	061612	
12)	.000000	106667	
13)	.000000	079085	
14)	.000000	077296	
15)	.000000	061256	
16)	.000000	063088	
17)	.000000	098625	
18)	.000000	112024	
19)	.000000	150044	
20)	.000000	091064	
21)	.000000	062598	

NO. ITERATIONS= 9

RANGES IN WHICH THE BASIS IS UNCHANGED:

OBJ COEFFICIENT RANGE				
VARIAB			WABLE AI	LOWABLE
			DECREASE	
X11	14.000000	INFINITY	2.432912	
X21		4.626315		
X12		INFINITY		
X22	18.000000	7.004553	INFINITY	
X13		INFINITY		
X23	19.000000	4.004552	INFINITY	
X14	17.000000	7.995447	INFINITY	
X24	20.000000	INFINITY 1.996966 INFINITY	7.995447	
X15	8.000000	1.996966	INFINITY	
X25	10.000000	INFINITY	2.995448	
X16	12.000000	7.995447	INFINITY	
X26	13.00000	TIALITALI I	1.773441	
X17		7.995447	INFINITY	
X27	15.000000	INFINITY	7.995447	
X18	14.000000		3.002276	
X28	17.000000	6.004553	INFINITY	
X19	14.000000	T 00 T 1 1 T	NA VALUE VALUE V	
X29	17.000000	INFINITY	7.995447 INFINITY .495052 3.502276	
X110	15.000000	.330029	INFINITY	
X210	18.000000	INFINITY	.495052	
X111	15.000000	INFINITY	3.502276	
X211	18.000000	1.00	TY AT TY AT T	
X112	15.000000		3.502276	
X212	18.000000			
X113	15.000000	INFINITY	3.505430	
X213	18.000000	7.012784	INFINITY	
X114	16.000000	INFINITY	4.007208	
X214	19.000000	8.017712	INFINITY	
X115	16.000000	INFINITY	.025439	
X215	19.000000	.038212	INFINITY	
X116	17.000000		INFINITY	
X216				
	16.000000	.025480		
X217	19.000000	.495052	.038212	
	10.000000			
X218	12.000000	INFINITY	6.995447	

RIGHTHAND SIDE RANGES

ROW	CURREN	IT ALLOWA	BLE ALLOWABLI	Ξ
			DECREASE	
2	130.000000	INFINITY	10.784090	
3	130.000000	2.571191	5.030327	
	14707.000000	1846.130000	943.627000	
5	1318.000000	1894.421000	968.310400	
6	10964.000000	1566.947000	800.925900	
7	669.000000	721.455500	669.000000	
	1943.000000	379.599900	1943.000000	
9	459.000000	236.171500	459.000000	
10	462.000000	1311.022000	462.000000	
11	4284.000000	1795.827000	917.915000	
12	525.000000	1415.412000	525.000000	
13		2045.418000		
14	2618.000000	1496.522000	764.929200	
15	1314.000000	1888.385000	965.225000	
16	2770.000000	1833.554000	937.199000	
17	1046.000000	1223.879000	625.570700	
18	2142.000000	1077.496000	550.749000	
19	578.000000	1221.837000	578.000000	
20	2003.000000	1894.764000	677.508700	
21	639.000000	1722.758000	639.000000	